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# First discernments for NO storage and reduction (NSR) on lithium cuprate ( $Li_2CuO_2$ ) at moderate temperatures ( $100 \le T \le 400 \,^{\circ}C$ )



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#### ABSTRACT

The present study was carried out to analyze the NO storage and reduction (NSR) on  $\text{Li}_2\text{CuO}_2$ . The objective of this investigation was to determine the first insights of NSR, while using a new material.  $\text{Li}_2\text{CuO}_2$  was initially evaluated as NO sorbent (2 mL/min) in the presence of different oxygen contents. These results were used to verify the NO consumption and chemical sorption and to propose a reaction mechanism for the lithium nitrate formation. The best NSR results were obtained between 200 and 300 °C and  $\text{Li}_2\text{CuO}_2$  showed high stability during cycling processes. A reaction mechanism, based on the Mars–Van Krevelen model was presented. After that, similar experiments were performed but using a lower NO concentration (777 ppm), where the results were equivalent to those obtained with higher NO concentrations. Thus, results establish interesting bases to analyze and allow to a double NO NSR-SCR process in the future, using alkaline ceramics.

## 1. Introduction

In the last two decades, one of the most threatening global problems is related to different energetic and environmental issues [1]. Within this big issue, the pollution produced by nitrogen oxides (NO, NO<sub>2</sub> and N<sub>2</sub>O), chemically generalized as NO<sub>x</sub>, contribute to a series of environmental problems, although they are not the polluted gases with the highest concentrations on the atmosphere [2–4]. Nitrogen oxides are produced on stationary industrial installations, such as coal-consuming power plants and industrial boilers, among others [5], and they are responsible for the photochemical smog and the acid rain [6]. Based on that, the scientific community has established different approaches for the NO<sub>x</sub> elimination: i) the NO<sub>x</sub> storage and reduction (NSR), which implies the NO<sub>x</sub> oxidation and separation as nitrites or nitrates and ii) NO<sub>x</sub> selective catalytic reduction (SCR), implying a simultaneous sorption and catalytic reaction with other species such as carbon monoxide (CO) or ammonia (NH<sub>3</sub>) [7–12].

For the NSR process, NO is oxidized to  $NO_2^{1-}$  or  $NO_3^{1-}$  species, producing nitrites or nitrates, respectively. This reaction mechanism is mostly performed over noble metals in presence of a basic compound [13–15]. In general, the materials used for this application have the following chemical content; nobel metal/BaO/ceramic support, where the nobel metal is usually platinum, while the ceramic supports are alumina (Al<sub>2</sub>O<sub>3</sub>) or ceria (CeO<sub>2</sub>) [13,16–20]. About the basic compound, most of the reports published on literature used barium or

strontium oxides, and only a few other reports used some perovskites with lower basic properties [21–25]. Therefore, the development and analysis of different materials, as possible variants for the nobel metal and barium oxide materials would be of great interest from several points of view.

Recently, the application of copper-containing materials, not for the NSR process, but for the carbon monoxide selective catalytic reduction (CO-SCR) of NO has been reported [26–28]. These materials have received extensive attention, as in several cases, the presence of novel metals are not needed. For example, it has been demonstrated that CuO particles deposited on titania (TiO<sub>2</sub>) supports have excellent activity in the CO-SCR reaction [29]. More recently, as another example, it was reported that copper nanoparticles deposed over carbon supports are able to perform the NH<sub>3</sub>-SCR reaction process at moderate temperatures [27]. Thus, copper-containing materials seem to possess good properties for the NO selective catalytic reduction process.

On the other hand, lithium cuprate  $(\text{Li}_2\text{CuO}_2)$  is a highly alkaline ceramic, which has been proposed for different applications such as lithium-ion batteries [30–32] and as  $\text{CO}_2$  and CO captor material [33–35].  $\text{Li}_2\text{CuO}_2$  has a laminar structure formed by [ $\text{CuO}_4$ ] plane squares and lithium cations located into the interlayer spaces [36,37]. This crystal structure produces a high lithium cation mobility, which is the main reason for using  $\text{Li}_2\text{CuO}_2$  in these applications. Moreover, the gas sorption applications have been established based on the same

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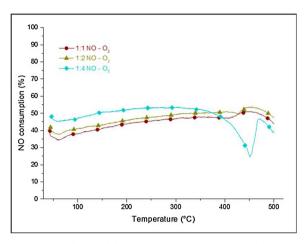
lithium cation mobility, but as well on the basic particle surface and redox cupper properties [33,35]. Based on all the previous descriptions, the aim of this work was to analyze the NO possible consumption and sorption on  $\text{Li}_2\text{CuO}_2$ , in the presence of different amounts of oxygen. This work is presented as a first insight of the possible utilization of this lithium ceramic within the NO<sub>x</sub> reduction process, either under the NSR and/or SCR schemes.

## 2. Experimental section

 ${\rm Li_2CuO_2}$  sample was obtained by solid-state reaction where the precursors, lithium oxide (Li\_2O, Aldrich) and copper oxide (CuO, Meyer), were mechanically mixed and heated at 800 °C for 6 h in air [38]. It was characterized by X-ray diffraction (XRD) and fitted with 01-073-2324 JCPDS file, which corresponded with the Li\_2CuO\_2 orthorhombic crystalline phase. Moreover, the  ${\rm N_2}$  adsorption-desorption isotherm of the sample was obtained to determine the BET specific surface area of the sample;  $2.0~{\rm m^2/g}$  (data not shown). Finally, the pristine  ${\rm Li_2CuO_2}$  was characterized by X-ray photoelectron spectroscopy (XPS), using a KAlpha Thermo Scientific spectroscopy equipment. It provided an X-ray source and  ${\rm Al-K_{\alpha}}$  monochromatic radiation. An argon beam was used to eliminate sample surface impurities. Moreover, the  ${\rm C_{1s}}$  peak (284.6 eV) was used for energy calibration.

Different gas sorption experiments were performed using a catalytic flow reactor (CATLAB-PCS, Hiden Analytical) coupled with QGA mass spectrometer (Hiden Analytical), using the following MS numbers for the NO, N2O and NO2 identification, 30, 44 and 46 amu, respectively. All these experiments were carried out using NO (Praxair, 2% N2 balanced), O2 (Praxair, grade 2.6) and N2 (Praxair, grade 4.8). N2 was used as a gas balance and as the carrier gas, using in all the experiments a total flow rate of 100 mL/min. Dynamic and isothermal profiles were obtained using 0.1 g of Li<sub>2</sub>CuO<sub>2</sub> in each experiment. For an initial set of experiments, dynamic experiments were performed from 30 to 500 °C. using different NO:O2 ratios (1:4, 1:2 and 1:1). Then, the isothermal analyses were carried out at different temperatures, between 100 and 450 °C. In the isothermal experiments, samples were heated to the desired temperature under a N2 flow (60 mL/min), and once each sample reached the corresponding temperature, the gas flow was switched to the corresponding gas mixture, with a total flow of 100 mL/min. The isothermal condition was kept during eight hours. After that, cyclic experiments (10 cycles) were performed at 300 °C, using the three different NO:O2 ratios during sorption (1 h) and N2-O2  $(P_{O2}:P_{N2} = 0.05:0.95)$  for desorption process at 650 °C during 1 h. The isothermal and cyclic Li<sub>2</sub>CuO<sub>2</sub> products were analyzed by XRD, ATR-FTIR and TG. The XRD patterns were obtained with a D5000 Siemens diffractometer coupled to a Co anode X-ray tube. Compounds were identified using the Joint Committee Powder Diffraction Standards (JCPDS) database. The ATR-FTIR spectra  $(4000-400\,\mathrm{cm}^{-1})$  were obtained using ALPHA-Platinum equipment from Bruker. Finally, the thermogravimetric analyses were performed from 40 to 850 °C in a thermogravimetric balance Q500HR, from TA Instruments in order to determine the presence of different species on the samples.

Based on the previous experiments, new experiments were performed at a lower NO concentration (777 ppm), simulating a real NO concentration. In this case, dynamic experiments were performed from 30 to 320 °C, varying the  $O_2$  contents (4, 6, 8, 10 mL/min). The isothermal experiments were obtained between 100 and 300 °C, only using 4 mL/min of oxygen for 180 min. Two different cyclic experiments were performed at 300 °C using 777 ppm of NO and 4 mL of oxygen in the sorption process, while the previously described  $N_2$ - $O_2$  gas mixture was used at 650 °C during the desorption process. The first cyclic experiment had 10 cycles, 1 h of sorption and 1 h of desorption. Conversely, the second cyclic experiment consisted of 5 cycles, which were performed during 8 h of sorption and 1 h of desorption. As in the first set of experiments, isothermal and cyclic sample products were analyzed by XRD.



**Fig. 1.** Dynamic evolution of the NO consumption as a function of temperature, varying the oxygen concentration.

#### 3. Results and discussion

As it was mentioned on the introduction section, Li<sub>2</sub>CuO<sub>2</sub> presents great basic chemical properties, probed by the CO and CO2 sorption capacities, two acid molecules [33]. Based on that, and the fact that NO is another acid gas, its sorption possibility, on Li<sub>2</sub>CuO<sub>2</sub>, was analyzed. Thus, different dynamic experiments, between 30 and 500 °C, were performed varying the NO:O2 ratio (Fig. 1). These initial experiments were performed using a NO concentration of 2 %, N2 balanced (see experimental section) in the presence of different amounts of oxygen. All the NO:O<sub>2</sub> ratios presented similar NO consumption trends between 30 and 320 °C, getting the best NO consumptions (around 50 %) when the NO:O<sub>2</sub> ratio was 1:4. Nevertheless, at higher temperatures (T ≤ 380 °C), this NO:O2 ratio importantly decreases the NO consumption, something almost not presented when lower O2 amounts were used. This result is produced by different factors: The amounts of NO sorbed saturated and blocked the Li<sub>2</sub>CuO<sub>2</sub> particle surface inhibiting further sorptions, but mainly due to the oxygen adsorption produced during the nitrate formation, which competes by the adsorption sites, as it is described below. Moreover, LiNO3 decomposes at this temperature range. So, the NO sorption-desorption equilibrium must be affected at T > 450 °C. It must be mentioned that during these experiments all the other possible NO<sub>x</sub> gases were followed by the mass spectrometer, not observing any of them (data not shown).

Based on the dynamic results, all the NO:O2 ratios were isothermally tested, to further analyze the process. Fig. 2 shows the results obtained when the NO:O2 ratio was 1:4, in order to deeply visualize, analyze and understand the NO sorption and consumption evolution processes on  $\text{Li}_2\text{CuO}_2$ . The isotherm performed at 100 °C presented a continuous NO consumption of ~49 %, being highly stable during the whole isothermal process (480 min). Then, the isotherm performed at 200 °C presented similar stability, although the NO consumption was importantly higher, 70 %. In fact, at this thermal condition, the NO consumption presented its highest value. Isotherms performed between 250 and 350 °C decreased the NO consumption between 65 and 50 %. Then, the NO consumption decrement continued as a function of temperature, as the isotherms obtained at 400 and 450 °C presented the lowest values. The differences observed between the isotherms and the dynamic experiments (see Fig. 1) can be explained by the different equilibrium regimes present in each experimental set; non-equilibrium and equilibrium systems are presented during the dynamic and isothermal experiments respectively.

All the isothermal Li<sub>2</sub>CuO<sub>2</sub> products were analyzed by XRD and ATR-FTIR. These results are presented in Fig. 3. The XRD patterns presented an evolution of the crystalline phases as a function of temperature (Fig. 3-A). Between 100 and 250  $^{\circ}$ C, it is clearly evident that

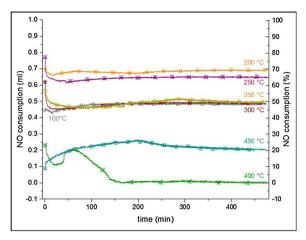
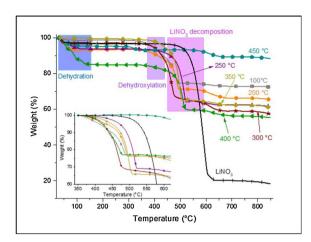


Fig. 2. Dynamic evolution of NO obtained during the isothermal processes performed on  $\rm Li_2CuO_2$  at different temperatures. The NO:O ratio used for these isotherms was 1:4.

Li<sub>2</sub>CuO<sub>2</sub> tended to decrease, while CuO (JCPDS file 00-005-0661) increased. In none of these cases was possible to determine any lithium secondary phase, despite the CuO formation. In fact, at 300 °C, the only phase detected in the corresponding diffraction pattern was CuO, indicating that Li<sub>2</sub>CuO<sub>2</sub> is being consumed. Then, between 350 and 400 °C it was possible to identified lithium nitrate (LiNO3, JCPDS file 01-080-0203) as a lithium containing crystal phase, confirming the NO chemical sorption on Li<sub>2</sub>CuO<sub>2</sub>. Finally, at 450 °C Li<sub>2</sub>CuO<sub>2</sub> was the unique crystal phase obtained, in good agreement with the low NO consumption observed dynamic and isothermally at this temperature. Something else must be pointed out from these XRD patterns. The CuO diffraction peaks are importantly wide in all the cases, indicating the formation of nanocrystals. Thus, the CuO crystal sizes were determined by using the Scherrer equation [39]. The corresponding measurements indicated that CuO crystals grew from 240 to 453 Å, while increasing the isothermal temperature from 100 to 400 °C. Thus, the formation of CuO nanocrystals must be related to the Li<sub>2</sub>CuO<sub>2</sub> partial and continuous degradation produced by the NO chemical sorption, while CuO crystal growth must simply be attributed to the temperature in which each isothermal experiment was performed.

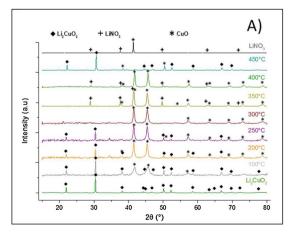
The NO chemical sorption was corroborated by ATR-FTIR (Fig. 3-B). The characteristic vibrations of the N–O bond were identified on the  $\rm Li_2CuO_2$  isothermal products obtained between 200 and 400 °C. An anti-symmetrical vibration mode of stretching is located at 1380 cm $^{-1}$ , and this energy absorption is considered the most intense. Although the symmetric vibration mode is inactive in infrared, there are two modes



**Fig. 4.** Decomposition thermograms of the Li<sub>2</sub>CuO<sub>2</sub> isothermal products obtained after the NO:O<sub>2</sub> process, where the NO:O ratio was 1:4. The square inset shows a normalized amplification of the nitrate decomposition temperature range.

of angular deformations for O–N–O bonds in infrared at 830 and  $720\,\mathrm{cm}^{-1}$ . Besides, the bands associated with monodentate nitrates at approximately  $1035\,\mathrm{cm}^{-1}$  were presented [40,41]. Then, although LiNO<sub>3</sub> was not identified on the XRD patterns obtained at T <  $300\,^{\circ}$ C, it was possible to identify it by ATR-FTIR. It may be simply explained based on the LiNO<sub>3</sub> dispersion or crystal sizes produced over the Li<sub>2</sub>CuO<sub>2</sub> surface particles. Moreover, the ATR-FTIR spectra confirmed that LiNO<sub>3</sub> was not formed at 450 °C, as it was shown by the corresponding XRD pattern. It must be mentioned that some other bands were detected, in addition to the nitrate vibration bands. These vibration bands were attributed to  $\mathrm{CO_3^{2-}}$  (860 cm<sup>-1</sup>) and  $\mathrm{OH^{1-}}$  (3600 – 3540 cm<sup>-1</sup>) species [42]. The presence of these carbonates and hydroxides ions must be simply explained by the carbonation and hydration-hydroxylation produced during the environmental atmospheric manipulation of the Li<sub>2</sub>CuO<sub>2</sub> sample products.

To complement the Li<sub>2</sub>CuO<sub>2</sub> isothermal product characterization, all of them were analyzed by TG analysis (Fig. 4). All these products presented three different weight loss attributed to dehydration (T  $\leq$  100 °C), dehydroxylation (between 380 and 440 °C) and denitration (T  $\geq$  450 °C). The first two processes (dehydration and dehydroxylation) must correspond to water sorbed on the products during the sample air exposition produced after the isothermal processes. In fact, LiNO<sub>3</sub> is highly hygroscopic. So, the isothermal sample produced at 400 °C, presenting the largest amount of lithium nitrate, was the sample more hydrated. This TG result is in good agreement with all previous



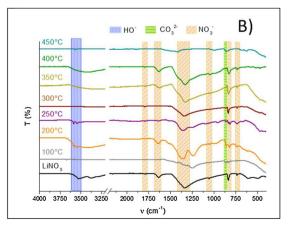


Fig. 3. XRD patterns (A) and ATR-FTIR spectra (B) of the  $\text{Li}_2\text{CuO}_2$  isothermal products obtained after the NO:O<sub>2</sub> process, where the NO:O ratio was 1:4. The pristine  $\text{Li}_2\text{CuO}_2$  and  $\text{LiNO}_3$  patterns and spectra are included for comparison purposes.

results. Then, the denitration process corresponds to the LiNO $_3$  decomposition. In fact, the pristine LiNO $_3$  decomposition was incorporated on this figure, for comparison purposes. The amounts of weight loss attributed to denitration process were between 22 and 34 wt%, although the Li $_2$ CuO $_2$  sample product obtained at 450 °C practically did not present this weight loss. Again, these results confirm that NO is being chemically trapped on Li $_2$ CuO $_2$ , but the NO chemisorption is only produced between 100 and 400 °C.

All these results confirmed that Li<sub>2</sub>CuO<sub>2</sub> is able to trap, chemically, NO between 100 and 400 °C, obtaining the highest NO consumptions at around 200 - 250 °C. The most probable reaction mechanism may be the Mars-van Krevelen reaction mechanism model [43], which is well accepted for oxidation processes involving reducible metal oxides. In fact, this model has been already proposed for the carbon monoxide chemisorption on lithium cuprate and other lithium ceramics [35,44]. In fact, it is well known that lattice oxygen mobility and release are highly important in the Mars-van Krevelen model. Based on that the XPS spectrum of Li<sub>2</sub>CuO<sub>2</sub> was obtained to determine its oxygen binding energy (see supplementary Figure S1). The O(1 s) binding energy was measured at 532.0 eV, which is a similar but slightly higher value than those values reported for copper oxides; CuO (529.5 eV) and Cu2O (530.5 eV) [45]. It means that oxygen binding energy on Li<sub>2</sub>CuO<sub>2</sub> should have similar release availability than copper oxides, which have excellent characteristics. Thus, this model implies that NO is adsorbed on the Li<sub>2</sub>CuO<sub>2</sub> surface, which releases oxygen anions. Moreover, these anionic vacancies must be immediately occupied and used for the O2 adsorption and homolytic dissociation, completing the lithium nitrate formation. This general process is presented in reaction 1.

$$\text{Li}_2\text{CuO}_2 + 2 \text{ NO} + 1.5 \text{ O}_2 \longrightarrow 2 \text{ LiNO}_3 + \text{CuO}$$
 (1)

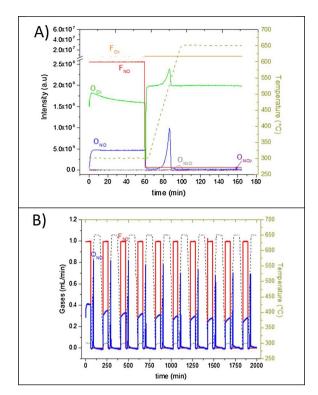
The assumption that NO is adsorbed with the subsequent oxygen release, from the  $\text{Li}_2\text{CuO}_2$  crystal structure, is based on the following two facts; i) that lithium cuprate was able to consume NO, even in the absence of oxygen (data not shown). In such a case, copper must be reduced to metallic copper, releasing all the oxygen anions from the lithium cuprate crystal structure. ii) It has been reported on literature that  $\text{Li}_2\text{CuO}_2$  has high reducibility properties. It was evidenced through CO-TPR, TG and catalytic experiments [33,35]. In those cases, it was shown that  $\text{Cu}^{2+}$ , initially contained on the  $\text{Li}_2\text{CuO}_2$  crystal structure, can be easily reduced to  $\text{Cu}^{1+}$  or  $\text{Cu}^0$ , due to oxygen release. Thus, the whole NO reaction evolution performed on  $\text{Li}_2\text{CuO}_2$ , through the Mar — Van Krevelen mechanism, is summarized in reactions 2 to 4:

$$NO \xrightarrow{Li_{2}CuO_{2}} NO_{2}^{1-} + Li_{Li} + Cu_{Cu}^{\bullet \bullet} + V_{o}^{"}$$
 (2)

$$V_o^{"} + O_{2(g)} \to 2O^{\bullet}$$
 (3)

$$NO_2^{1-} + O^{\bullet} \to NO_3^{1-}$$
 (4)

In order to analyze the reproducibility of NO sorption and Li<sub>2</sub>CuO<sub>2</sub> stability, different cyclic experiments were performed analyzing the gas evolution during cycles as well as the sample composition at the end of the whole process. Fig. 5-A shows the evolution of NO, other possible NO<sub>x</sub> and O<sub>2</sub> gases as a function of temperature, during the first cycle. In the first hour, at 300 °C, the determined amounts of NO (O<sub>NO</sub>) and O<sub>2</sub> (O<sub>O2</sub>) consumed were relatively constants, showing good consumption stability of the process. They were based on the few NO (F<sub>NO</sub>) and O<sub>2</sub> (FO2) amounts. Then, as soon as the NO flow was closed and temperature began to increase, there was a sudden but important O2 consumption, suggesting high oxygen sorption on the Li<sub>2</sub>CuO<sub>2</sub> sample, with the subsequent oxygen stabilization. This high oxygen consumption indicates the deficiency of this element on the Li<sub>2</sub>CuO<sub>2</sub> sample product after the NO flow, which must be produced due to the NO oxidation to nitrates, as explained above. After that, during the heating process (between 450 and 540 °C), the sample evidenced the NO and  ${\rm O}_2$  desorptions. This result shows that reaction 1 is reversible at high



**Fig. 5.** Dynamic evolution of gases produced during the sorption and desorption cyclic experiment. The first cycle (A) presents NO and  $O_2$  volume feeds ( $F_{NO}$  and  $F_{O2}$ ) as well as the corresponding concentrations at the sweep ( $O_{NO}$  and  $O_{O2}$ ). Moreover, the  $N_2O$  and  $NO_2$  production were followed. Ten cycles curve (B) only shows the NO evolutions.

temperatures in the oxygen presence, of course. Finally, it must be mentioned that  $\rm N_2O$  desorption was observed between 550 and 650 °C, while  $\rm NO_2$  was never detected, unless it had rapidly evolved to NO. In such a case, it would be involuted as part of the NO signal. The presence of small amounts of  $\rm N_2O$ , after most of the NO desorption, indicates that residual amounts of lithium nitrate decompose as it is shown in reaction 5, where the produced  $\rm Li_2O$  must react with CuO regenerating  $\rm Li_2CuO_2$ , during the same heating process. After the analysis of the first cycle, ten new cycles were performed consecutively (Fig. 5-B). The  $\rm Li_2CuO_2$  sample presented good stability during all these cycles, as the amounts of NO consumed and desorbed only presented a slight decrement after 10 cycles.

$$2 \text{ LiNO}_3 \rightarrow \text{N}_2\text{O} + \text{Li}_2\text{O} + 2 \text{ O}_2$$
 (5)

The cyclic experiment was repeated varying the oxygen content, where the results showed two different trends. In one hand, independently of the  $NO:O_2$  ratio the NO consumption increased as a function of the cycles. It must be attributed to the Li<sub>2</sub>CuO<sub>2</sub> microstructural evolution produced on these materials after the gas chemical sorption and crystal regeneration [46]. On the other hand, it can be seen that high NO sorption-desorption stabilities for all the NO:O2 ratios, where the oxygen concentration slightly increases the cyclic efficiency (Fig. 6-A). After the different cyclic experiments, all the Li<sub>2</sub>CuO<sub>2</sub> products, after a final NO desorption step, were re-analyzed by XRD and compared with the pristine Li<sub>2</sub>CuO<sub>2</sub> and LiNO<sub>3</sub> samples (Fig. 6-B). Independently of the oxygen content, all the Li<sub>2</sub>CuO<sub>2</sub> cyclic products were composed of Li<sub>2</sub>CuO<sub>2</sub> and CuO. This result shows that part of the Li<sub>2</sub>CuO<sub>2</sub> is been decomposed through the cycles. The Li<sub>2</sub>CuO<sub>2</sub> partial decomposition must be produced during the heating NO desorption process, where lithium may have sublimed. This assumption is supported by the N<sub>2</sub>O desorption, which implies the Li<sub>2</sub>O production (see reaction 2), which must be mostly reincorporated into the Li2CuO2

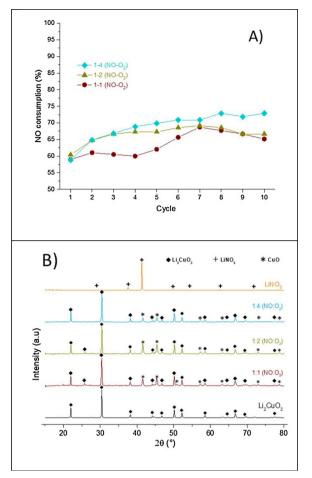
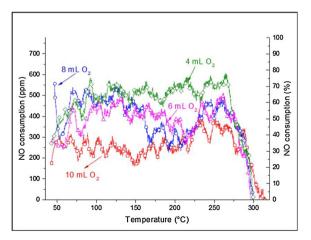


Fig. 6. NO consumption efficiencies (A) and XRD patterns of the  $\rm Li_2CuO_2$  cyclic products (B) obtained using different NO:O<sub>2</sub> ratios. The pristine  $\rm Li_2CuO_2$  and  $\rm LiNO_3$  patterns are included for comparison purposes.

crystal structure, but part of it must have sublimed as well, as it is well known [35].

After the whole analysis performed on  ${\rm Li_2CuO_2}$  for the NO sorption, using a high NO concentration, the same analysis was performed, but using a much lower NO concentration (777 ppm), which is a close concentration than that presented in real gas polluted systems. Then, as in the previous cases showed above, dynamic experiments were initially performed varying the  ${\rm O_2}$  content (Fig. 7). All these systems presented



**Fig. 7.** Dynamic evolution of the NO consumption as a function of temperature, using a low NO concentration (777 ppm) and varying the oxygen contents.

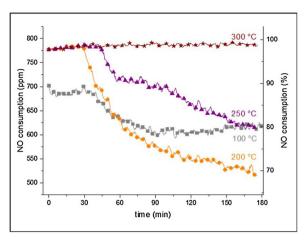


Fig. 8. Dynamic evolution of NO (777 ppm) obtained during the isothermal process performed on  $\rm Li_2CuO_2$  at different temperatures, using 4 mL/min.

important NO consumptions, depending on the oxygen content, where the best NO consumptions (around 70 %) were observed with an  $\rm O_2$  flow content of 4 mL/min. It must be noticed that the NO consumption tended to decreased when the  $\rm O_2$  contents increased. It seems that high oxygen concentration inhibits the NO consumption, probably as there may be an adsorption sites competition between the two gases. Furthermore, the NO consumption tended to decrease at temperatures higher than 275 °C, independently of the oxygen content. This is a similar behavior than that observed with a larger NO concentration. Nevertheless, in this case, the NO consumption decrement was observed at a lower temperature. This thermal shift can be explained based on the NO sorption-desorption equilibrium, which was shifted to a lower temperature due to the low NO concentration.

Based on the NO sorption dynamic results, different isothermal experiments were performed between 100 and 300 °C using 4 mL/min of oxygen (Fig. 8). At 100 °C, the isothermal trend decreased from 90 to 80 % of efficiency through the 180 min. Then, at higher temperatures, the initial NO consumption was total (100 %), at least during the first minutes. However, isotherms performed at 200 and 250 °C only showed a total NO consumption during the initial 30 – 40 min, decreasing to 70 and 80 % of efficiency after 3 h, respectively. Conversely, the isothermal experiment performed at 300 °C presented a 100 % of efficiency during all the experimental time. Here, the high NO consumption should be attributed to its low concentration, in comparison to the NO high concentration results observed above, where the LiNO<sub>3</sub> production must have saturated the Li<sub>2</sub>CuO<sub>2</sub> surface. In these cases, the XRD and ART-FTIR results did not evidence clearly the presence of LiNO<sub>3</sub> (see supplementary Figure S2), although the presence of CuO confirmed that Li<sub>2</sub>CuO<sub>2</sub> did partially reacted with NO. Thus, the LiNO<sub>3</sub> must be highly dispersed ad out of the detection limit of this technique. Complementarily, the ATR-FTIR spectra of these isothermal products slightly depicted the corresponding nitrate vibration bands. However, another isothermal experiment was performed at 300 °C during 12 h, where a whole efficiency (100 %) was maintained. Moreover, the XRD pattern and ATR-FTIR spectrum of that isothermal Li<sub>2</sub>CuO<sub>2</sub> product did show the formation of LiNO<sub>3</sub> (see supplementary Figure S3).

Based on the fact that  $\rm Li_2CuO_2$  was able to trap NO isothermally, even at low concentrations, two different sets of cyclic experiments were performed, where the NO consumption times were varied. In the first case, identical NO sorption-desorption conditions were used, in comparison to those conditions used with the high NO concentration. Fig. 9 shows that NO and  $\rm O_2$  presented the same trends than those described above, using a high NO concentration. Of course, the amounts of NO consumed were slightly higher in this case, because the ceramic is able to trap more NO during longer times, due to the lower concentration. However, the efficiency of NO consumption varied when

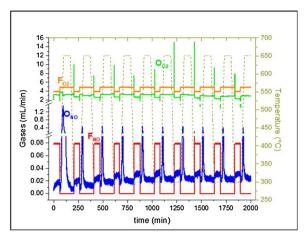


Fig. 9. Dynamic evolution of NO and  $O_2$  produced during the sorption (1 h) and desorption (1 h) cyclic experiment, using a low NO concentration (777 ppm). NO and  $O_2$  volume feeds ( $F_{NO}$  and  $F_{O2}$ ) as well as the corresponding concentrations at the sweep ( $O_{NO}$  and  $O_{O2}$ ) are presented.

the NO concentration was reduced, moving 65-70% to 80-85%, while the NO concentration decreased. It may be explained base on the fact of an adsorption sites unsaturation, allowing to higher efficiencies.

Something important must be taken into account for the cyclic experiments. In the NO low concentration case, the possible amount of LiNO<sub>3</sub> produced during the sorption step is importantly low. Thus, longer NO sorption time may be expected and performed. Based on that, a second cyclic experiment was performed, but in this case, the NO consumption time was 8 h (Fig. 10). The general trend was similar to previous cases. Nevertheless, the NO sorption time allowed to evidence how the amounts of NO at the exit (ONO) increased as a function of time, from almost zero to 0.02 - 0.025 mL/min (Fig. 10-A). This change must be attributed to a partial NO sorption saturation presented by the Li<sub>2</sub>CuO<sub>2</sub> sample through the time. Then, when the two sets of cyclic experiments are compared different issues must be pointed out (Fig. 10-B). First, when the NO consumption is compared as a function of the cycle number, the experiments showed NO consumptions between 85 and 76 %, where the short time cycles apparent better consumptions. Nevertheless, it must be taken into account that one long time NO consumption cycle is sorbing much longer amounts of NO. These larger NO amounts, which must be associated to LiNO3 and CuO formation, should slightly decrease the average NO consumption during one cycle process. Thus, when the cycles are compared as a function of time (square inset of Fig. 10-B), it is more evident that long NO consumption cycle processes converting more NO amounts, even though this experiment only was performed during five cycles.

Finally, after both cyclic experiments, the  $\rm Li_2CuO_2$  sample products were analyzed by XRD, and compared, again, with pristine  $\rm Li_2CuO_2$  and  $\rm LiNO_3$  (Fig. 11). As it would be expected, the  $\rm Li_2CuO_2$  cyclic products obtained after the larger NO sorption steps evidenced a higher lithium cuprate partial decomposition, as the amounts of CuO were more evident. This result suggests a larger  $\rm Li_2O$  sublimation produced during the  $\rm LiNO_3$  decomposition, as explained above.

## 4. Conclusions

In the present work, the NO storage and reduction on  $\rm Li_2CuO_2$  was analyzed, using different physicochemical conditions. First, and in order to determine the NO reactivity with  $\rm Li_2CuO_2$ , a relatively large NO concentration was used,  $\rm 2\,mL/min$  in the presence of different amounts of oxygen (N<sub>2</sub> balanced to total flows of  $\rm 100\,mL/min$ ). Different dynamic and isothermal experiments were performed, where relatively high NO consumption efficiencies were observed, without the formation of any other  $\rm NO_x$  specie. The NO consumption was confirmed

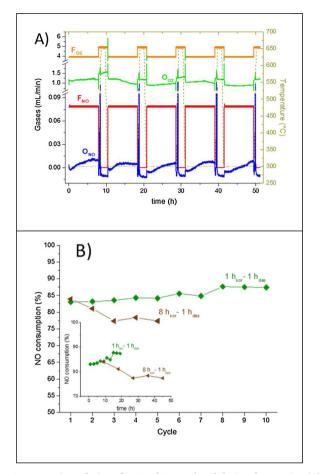


Fig. 10. Dynamic evolution of NO and  $O_2$  produced during the sorption (8 h) and desorption (1 h) cyclic experiment (A), using a low NO concentration (777 ppm). NO and  $O_2$  volume feeds ( $F_{NO}$  and  $F_{O2}$ ) as well as the corresponding concentrations at the sweep ( $O_{NO}$  and  $O_{O2}$ ) are presented. NO consumption comparison as a function of the cycles and sorption time (B).

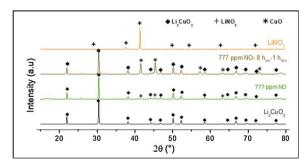


Fig. 11. XRD patterns of the different  $\rm Li_2CuO_2$  cyclic products using a low NO concentration (777 ppm), where the pristine  $\rm Li_2CuO_2$  and  $\rm LiNO_3$  patterns are included for comparison purposes.

by the  ${\rm Li_2CuO_2}$  isothermal products analyses, which were performed by XRD, ATR-FTIR and TG analyses. All these techniques evidenced the formation of  ${\rm LiNO_3}$  and  ${\rm CuO}$  produced due to the NO chemical capture process performed on  ${\rm Li_2CuO_2}$ . All these experimental data allowed to determining and proposing a reaction mechanism, based on the Mars–van Krevelen reaction model, well accepted for oxidation processes involving reducible metal oxides. After that, a cyclic experiment was performed to determine the  ${\rm Li_2CuO_2}$  stability. Results evidence a high NO chemical sorption during ten cycles, and it was observed that during  ${\rm LiNO_3}$  decomposition, NO is mainly produced although small amounts of  ${\rm NO_2}$  were detected.

After evidencing the NO consumption and chemical reaction with  $\rm Li_2CuO_2$ , a second set of experiments were performed, but using a lower NO concentration (777 ppm), trying to simulate a NO concentration or real gas flows. Results showed that  $\rm Li_2CuO_2$  is able to consume NO in similar averages than those presented before. Nevertheless, the NO consumption times were extended as the  $\rm Li_2CuO_2$  particles surface saturation with  $\rm LiNO_3$  did not occur at least during 8 h of NO consumption. All these results proved that  $\rm Li_2CuO_2$  is able to perform the NSR process, and it would be considered as a possible candidate for NO sorption and selective catalytic reduction (NSR-SCR) as well.

## CRediT authorship contribution statement

Ana Yañez-Aulestia: Data curation, Formal analysis, Investigation, Methodology, Writing - original draft, Writing - review & editing. Heriberto Pfeiffer: Conceptualization, Formal analysis, Funding acquisition, Investigation, Methodology, Project administration, Resources, Supervision, Visualization, Writing - original draft, Writing - review & editing.

### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Appendix A. Supplementary data

Supplementary material related to this article can be found, in the online version, at doi:https://doi.org/10.1016/j.apcatb.2020.119119.

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